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基于 HPSO 的供水管网摩阻因数反演

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摘要:由于运行中管道实际摩阻因数与设计采用值的不一致会影响供水系统的运行质量和安全,为得到准确的摩阻因数以反馈设计,以及对运行中的供水系统进行系统诊断和优化调度,提出一种基于混合粒子群优化算法(hybrid particle swarm optimization,HPSO)和管网水力计算模型的管段摩阻因数智能反分析方法,该方法以监测点处的水压监测值与水力计算模拟水压值的二乘误差最小为目标,通过 HPSO 的强大全局寻优能力计算不同管段的摩阻因数。对室内试验管网模型的反演结果表明:采用正常工况下反演得到的摩阻因数模拟水压监测点处水压与实际测量值之间误差最大为 2.87%;在爆管工况下,水压模拟值与实际测量值最大相对误差为 2.63%,说明通过该方法进行摩阻因数的反演具有较强的稳定性。

关键词:供水管网;混合粒子群算法;节点水压法;摩阻因数;反演;爆管监测

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供水管网是城市的生命线工程,在乡村振兴战略实施和农村饮水安全保障及城乡供水一体化工程加速建设的背景下,供水管网也已成为广大农村的生命线工程^[1-2]。为保质保量且经济合理地完成供水任务,需要对供水管网进行科学规划设计和精准优化调度。供水管网的水力模拟计算是管网规划、设计、运行调度和故障诊断的基础,而在影响管网水力计算模型准确性的因素中,摩阻因数的影响尤为突出^[3-6],如:新疆小洼槽倒虹吸工程采用的玻璃钢夹砂管在设计过程中所采用的糙率因数为 0.009 0,但在实际运行中测量得到糙率因数为 0.010 6,糙率因数选取过小,实际沿程水头损失增大,导致管道水压不够,输水流量达不到设计要求^[7];南水北调中线北京段 DN 4000 的 PCCP 管道,曼宁糙率系数实测值较设计值小 15%,实际运行水头损失为设计值的 69%^[8]。因此,管道摩阻因数具有较强不确定性且随时间动态变化,若能根据已知的水流条件和管网

的部分节点水压(或流量)监测值反演各管段的实际摩阻因数,以弥补原型管网与水力仿真模型间的差异,可使水力模拟结果更贴近实际情况,从而有效地反馈设计和指导运行。

管道摩阻因数的反演属于系统辨识中的参数辨识问题,且反演量(摩阻因数)与观测量(监测节点处水压等)间呈非线性关系^[4]。此类问题大多采用优化方法进行反演,而传统的基于梯度的优化算法常常遇到不收敛或收敛于局部极值的问题,因此,本文提出一种基于混合粒子群优化算法(hybrid particle swarm optimization,HPSO)和节点水压法相结合的摩阻因数反演方法^[9-12]。因现行设计标准中水头损失均按海森威廉公式计算^[13],故本文反演的摩阻因数为海森威廉(Hazen-Williams)因数。

1 基于 HPSO 的管网摩阻因数反演思路与方法

粒子群算法(particle swarm optimization,PSO)是

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由 Eberhart 等^[14]在 1995 年提出的连续非线性函数的优化方法,它是对鸟群或鱼群觅食过程中的迁徙和聚集的模拟,也可以说是对社会心理学的一种模拟^[15]。PSO 算法通过迭代,最终转化为求极值的问题,用适应度函数评估结果质量。PSO 算法存在易陷入局部最优、后期收敛速度慢及收敛精度差等缺点^[16],人们^[17-20]不断提出改进算法,如混合粒子群优化算法(HPSO)、自适应粒子群优化算法(APSO)等。本文引入改进的混合粒子群优化算法来对给水管网进行反演。

1.1 混合粒子群算法

Lovbjerg 等^[21]提出遗传算法结合混合粒子群模型,在粒子的搜索过程中加入遗传算法中交叉的过程。HPSO 模型对每次产生的新一代粒子群随机选择两个粒子进行交叉并进行适应度评价,保留适应度高的粒子位置与速度矢量并替换另一个粒子低适应度位置,提高全局和局部的搜索能力以及收敛速度。

设在 D 维空间中有 n 个微粒,其子代粒子的位置和速度矢量为

$$\vec{x}_1(t+1) = \vec{p} \cdot \vec{x}_1(t) + (1.0 - \vec{p}) \cdot \vec{x}_1(t) \quad (1)$$

$$\vec{x}_2(t+1) = \vec{p} \cdot \vec{x}_2(t) + (1.0 - \vec{p}) \cdot \vec{x}_2(t) \quad (2)$$

式中: $\vec{x}_1(t)$ 和 $\vec{x}_2(t)$ 表示 D 维空间的两个父代的位置向量; $\vec{x}_1(t+1)$ 和 $\vec{x}_2(t+1)$ 表示 D 维空间中下一代的位置向量; \vec{p} 是 D 维空间均匀分布的随机数向量, $\vec{p} \in [0, 1]$ 。

$$\vec{v}_1(t+1) = \frac{\vec{v}_1(t) + \vec{v}_2(t)}{|\vec{v}_1(t) + \vec{v}_2(t)|} \cdot |\vec{v}_1(t)| \quad (3)$$

$$\vec{v}_2(t+1) = \frac{\vec{v}_1(t) + \vec{v}_2(t)}{|\vec{v}_1(t) + \vec{v}_2(t)|} \cdot |\vec{v}_2(t)| \quad (4)$$

式中: $\vec{v}_1(t)$ 和 $\vec{v}_2(t)$ 表示 D 维空间的两个父代的速度向量; $\vec{v}_1(t+1)$ 和 $\vec{v}_2(t+1)$ 表示 D 维空间中下一代的速度向量。

每个微粒都有各自与优化目标函数 $f(x)$ 相对应的适应值,整个群体中微粒所经历过的具有最好适应度值的位置为 $P_{\text{best}} = (g_1, g_2, \dots, g_D)$ 。 $f(x)$ 的全局最优解按公式(5)计算。

$$f(P_{\text{best}}) = \min \{ f(P_1(t)), f(P_2(t)), \dots, f(P_n(t)) \} \quad (5)$$

微粒的速度是有所限制的,即 $v_i \leq v_{\text{max}}$ 。若某维的速度 $v_{id} > v_{id\text{max}}$ 则令 $v_{id} = v_{id\text{max}}$ ^[22-23]。HPSO 模型在达到最大迭代次数或小于允许最大流量闭合差时停止迭代。此时所有微粒都趋向同一点,即认为找到了最优位置^[24-26]。

1.2 基于 HPSO 的管网摩阻因数反演方法

管网海森威廉因数的反演由 HPSO 与管网水

力模拟计算两部分构成,其中 HPSO 完成优化功能,而针对 HPSO 生成的每一组摩阻因数组合均须调用基于节点水压法的管网的水力计算模型。具体步骤如下。

步骤 1 对 Hazen-Williams 因数 C 进行初始化,随机选取数值作为 HPSO 迭代的起始位置 x_{i0} 。

步骤 2 给定测点水压初值 $E_i^{(0)} (i=1, 2, \dots, m)$, 并将 x_{i0} 代入 Hazen-Williams 公式:

$$Q_{ij} = \frac{0.278 \ 53 x_{i0} \times D_{ij}^{2.63} h_{ij}^{0.54}}{L_{ij}^{0.54}}, i, j=1, 2, \dots, m \quad (6)$$

式中: Q_{ij} 为流量, m^3/s ; H_{ij} 为水头损失 $H_{ij} = E_i - E_j$; i, j 为节点编号; m 为节点数; L 为管长, m ; D 为管径, m 。

步骤 3 节点流量有如下公式:

$$f_i = Q_{ic} - Q_{ir} + q_i, i=1, 2, \dots, m \quad (7)$$

式中: f_i 为节点 i 处的流量闭合差, m^3/s ; Q_{ic} 为流出节点 i 的流量, m^3/s ; Q_{ir} 为流入节点 i 的流量, m^3/s ; q_i 为节点流量, m^3/s 。

计算 $f_i^{(0)} (i=1, 2, \dots, m)$, 如果所有节点均满足精度要求,即 $|f_i^{(0)}| < \epsilon$ (ϵ 为所需精度), 则 $E_i^{(0)}$ 为所求; 否则 $k = k + 1$, 做下一步节点水压校正。

步骤 4 由式(8)、(9)、(10)顺序求解可以依次得出水头的每一个校正值得 $\Delta E_i^{(k)} (i=1, 2, \dots, m)$, 并求出 E_i 新的近似值 $E_i^{(k+1)} = E_i^{(k)} + \Delta E_i^{(k)} (i=1, 2, \dots, m)$ 。

$$\begin{cases} \frac{\partial f_i}{\partial E_j} = a \sum_{j \in \varphi_i} R_{ij} |E_i - E_j|^{a-1}, i, j=1, 2, \dots, m \\ \frac{\partial f_i}{\partial E_i} = -a R_{ij} |E_i - E_j|^{a-1}, (\text{节点 } i \text{ 与 } j \text{ 相邻}) \\ \frac{\partial f_i}{\partial E_j} = 0, (\text{节点 } i \text{ 与 } j \text{ 不相邻}) \end{cases} \quad (8)$$

$$J = (J_{ij})_{m \times m} = \begin{bmatrix} \frac{\partial f_1}{\partial E_1} & \frac{\partial f_1}{\partial E_2} & \dots & \frac{\partial f_1}{\partial E_m} \\ \frac{\partial f_2}{\partial E_1} & \frac{\partial f_2}{\partial E_2} & \dots & \frac{\partial f_2}{\partial E_m} \\ \vdots & \vdots & & \vdots \\ \frac{\partial f_m}{\partial E_1} & \frac{\partial f_m}{\partial E_2} & \dots & \frac{\partial f_m}{\partial E_m} \end{bmatrix} \quad (9)$$

$$J^{(k)} \begin{bmatrix} \Delta E_1^{(k)} \\ \Delta E_2^{(k)} \\ \vdots \\ \Delta E_m^{(k)} \end{bmatrix} = - \begin{bmatrix} f_1^{(k)} \\ f_2^{(k)} \\ \vdots \\ f_m^{(k)} \end{bmatrix} \quad (10)$$

步骤 5 由公式(6)和(7)就可以计算得知 $E_i^{(k+1)}$ 即为所求解, 否则返回步骤 4。

步骤 6 将管网模型实际监测的节点水压值 E_{it} ($i=1, 2, \dots, m$) 与计算水压 E_i 之间的二乘误差的

平方根为适应值,并评价其适应度,即当 $f = \frac{\sqrt{\sum_{i=1}^m (E_{ki} - E_i)^2}}{m} < \epsilon_1$ (ϵ_1 为阈值)或达到一定迭代

次数则停止,否则按照前述步骤更新粒子群的速度矢量和位置矢量,搜索空间过往位置为最优,重新求解 E_i 新的近似值。

步骤 7 输出 Hazen-Williams 因数 C 。

2 基于室内试验模型的 Hazen-Williams 因数 HPSO 反演实例

2.1 室内试验模型

在室内设计建立一个包含 9 个基环的模型管网,为 2.5 m×2.5 m 的正方形平面管网。管网包含 18 个节点(含 1 个爆管点、1 个水塔),由 26 条长度为 1.0 m 或 0.5 m 的管段(外围管段直径均为 8 mm,内部管段直径均为 5 mm)和一条 2.3 m 的引水管段组成。管网包含 17 个出水口(16 个正常出水口、1 个爆管点)来模拟用户取水过程。在节点 1、4、13、16 处设置了水压的监测点,用 4 根带有刻度(精度为 0.1 mm)的测压管来观测 4 个监测点的水压值,各节点出流量 Q_i (mL/s)、管长 L (m)、管径 D (m),见图 1、2。

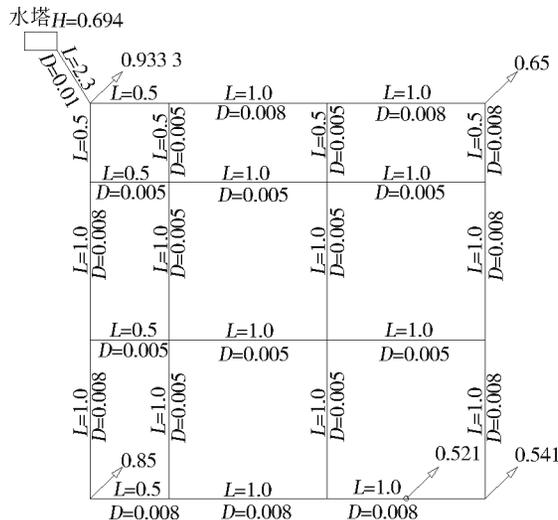


图 1 试验管网

Fig. 1 Test pipeline network

2.2 反演参数数量的确定

在反演问题中,反演量即未知量数量越多就需要更多的监测信息,故应尽量减少反演量的数量。在本文的管网模型中,正常工况下共有 25 个管段,异常工况(爆管时 $Q_{B_1} = 0.000\ 009\ 7\ m^3/s$)下有 26 个管段。由于采用同一种管材,所以影响摩阻系数 C 较大的因素为管段长度和管径,故将管长和管径相同的管道归为一类,第一类为 1、4、5、6、7、8、15、

22 管段,第二类为 26 管段,其余管段为第三类,需反演的海森威廉因数总数为 3 个。

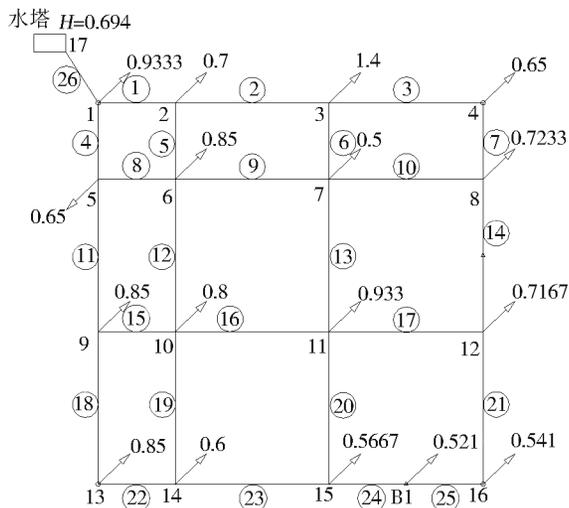


图 2 各节点与管段编号

Fig. 2 Number of each node and pipeline segment

2.3 摩阻因数的反演及结果分析

HPSO 算法通过监测得到的水压值进行反演计算得到摩阻系数 C 。HPSO 的优化目标 C_0 按式(11)计算。

$$C_0 = \frac{\sum \sqrt{(H_i - E_i)^2}}{4} \quad (i=1, 4, 13, 16) \quad (11)$$

式中: H_i 为节点的计算水压值, m; E_i 为监测水压值, m。

管网水力模拟的正向计算中,节点流量允许闭合差设定为 $0.000\ 001\ m^3/s$,最大迭代次数设定为 1 000。在反演过程中,粒子群数量为 15,最大迭代次数设定为 1 000,初始权重设为 0.85,权重以线性方式变化,终止迭代误差设为 $0.000\ 000\ 1$ 。

分正常工况和发生爆管两种情况进行试验,分别以相应的监测节点水压值进行优化反演,得到的海森威廉因数值见表 1,反演结果的相对误差在 $-7.07\% \sim 6.07\%$,说明不同工况下反演的因数具有较好的稳定性。以正常工况反演得出的摩阻因数重新分别计算正常工况及爆管工况下的监测节点的水压,并与试验监测值对比,其结果见表 2,最大相对误差绝对值为 2.87% 。

表 1 不同工况的 C 值及终止迭代误差

Tab. 1 C value and termination iteration error under different working conditions

| 管长/m | 正常工况下摩阻因数反演值 | B_1 点爆管时摩阻因数反演值 | 相对误差/% |
|------|--------------|-------------------|--------|
| 0.5 | 57.34 | 53.86 | 6.07 |
| 1.0 | 70.77 | 75.77 | -7.07 |
| 2.3 | 127.84 | 130.80 | -2.32 |

表 2 基于海森-威廉因数反演值重新模拟的监测节点水压与监测值的对比

Tab. 2 Comparison of monitoring node water pressure and monitoring value based on re-simulation of Hazen-Williams coefficient inversion value

| 节点 | 正常工况 | | | 爆管工况 | | |
|----|-------|-------|--------|-------|-------|--------|
| | 监测值/m | 计算值/m | 相对误差/% | 监测值/m | 计算值/m | 相对误差/% |
| 1 | 0.682 | 0.682 | 0.030 | 0.671 | 0.679 | 1.220 |
| 4 | 0.676 | 0.671 | -0.750 | 0.643 | 0.659 | 2.630 |
| 13 | 0.671 | 0.670 | -0.120 | 0.672 | 0.658 | -2.170 |
| 16 | 0.690 | 0.670 | -2.870 | 0.671 | 0.663 | -1.220 |

3 结 论

本文提出 HPSO 算法与管网水力计算节点水压法相结合进行管道摩阻因数的反演的思路与方法,针对室内试验模型进行反演计算与分析验证。得出以下结论:

HPSO 具有较强的全局寻优能力,正常工况和特殊工况(爆管)下反演得到的海森-威廉因数基本一致,相对误差为 -7.07% ~ 6.07% 。

以正常工况下的海森-威廉因数反演值计算正常工况及爆管工况下监测点的水压,其结果与实际水压监测值最大相对误差仅为 2.87% 。

实际中的管网水力参数是不断变化的,管段之间的摩阻因数也不尽相同。所以在供水系统运行过程中,应实时根据监测水压值修正摩阻因数,达到更好的模拟效果以及优化调度效果。另外,由于测量不确定度、监测点位置选取的不同等因素对反演结果有较大影响,需进一步加强监测点优化布置等方面的研究。

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Inversion of friction factor of water supply network based on HPSO

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Abstract: The water supply network is the lifeline project of the city. Under the background of the implementation of the rural revitalization strategy, the security of rural drinking water and the accelerated construction of the urban-rural water supply integration project, the water supply network has also become the lifeline project of the vast rural areas. In order to ensure the quality and quantity of water supply and complete the water supply task economically and reasonably, it is necessary to carry out scientific planning and design and precise optimization and scheduling of the water supply network. The hydraulic simulation calculation of the water supply network is the basis for the planning, design, operation scheduling and fault diagnosis of the pipeline network. Among the factors affecting the accuracy of the hydraulic calculation model of the pipeline network, the influence of the friction coefficient is particularly prominent. In order to narrow the gap between friction factor theory and practice, a calculation method based on hybrid particle swarm optimization algorithm and nodal water pressure method is proposed.

Hybrid particle swarm optimization model is obtained by combining the selection mechanism of basic particle swarm optimization and genetic algorithm. The difference between hybrid particle swarm optimization and particle swarm optimization lies in that the particle swarm has to cross operate after updating the velocity and position, and replace the parent particle with the offspring particle. The crossover operation makes the offspring inherit the advantages of the parent particles and theoretically strengthens the ability to search the region between the particles. In the algorithm, the initial friction resistance factor is randomly selected and put into the Hazen-William formula. The square root of the square error of the square error between the water pressures is calculated based on the actual water pressure value of the nodes monitored by the pipeline network model as the fitness value, and the fitness is evaluated. When the accuracy is met or the maximum number of iterations is reached, the frictional resistance factor is output.

In order to verify the feasibility of the method, a 2.5 m×2.5 m square flat pipeline network model was established in the laboratory experiment, which contained 9 basic rings. Four water pressure monitoring points are set in the model pipeline network node. Based on the friction resistance factor inversion under normal working conditions, the hydraulic simulation model of the pipeline network is established on this basis. In the case of pipe bursting, virtual nodes are introduced into the pipeline network model to simulate the pipe bursting point, and the simulation results are compared with the measured values to verify the accuracy of the model.

The results show that: (1) HPSO has a strong global optimization ability. The maximum relative error of the Hazen-Williams factor of each pipe section obtained by inversion under normal and special conditions (pipe burst) is 7%, with high accuracy and better adaptability. (2) Calculate the outlet water pressure of the monitoring point under the normal condition and the pipe burst condition with the inversion value of the Hazen-Williams factor under the normal condition. The maximum relative error between the result and the actual water pressure monitoring value is only 2.87%. The inverse problem solved by the method in this paper is well-posed.

Key words: water supply network; hybrid particle swarm optimization; nodal water pressure method; frictional resistance factor; the inversion; tube monitoring